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Techniques and Applications in Civil Engineering

PROCEEDINGS OF THE SECOND INTERNATIONAL CONFERENCE

Sponsored by The Engineering Foundation and The American Society of Civil Engineers **Technical Council on Computer Practices** Imaging Technologies Committee

Approved for publication by the Technical Council on Computer Practices of the American Society of Civil Engineers

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Abstract: This document is intended to provide the civil engineer with a comprehensive and up-to-date perspective on the use of imaging technologies for solving civil engineering problems. This proceedings includes the papers submitted to the Second International Conference on Imaging Technologies: Techniques and Applications in Civil Engineering, sponsored by the Engineering Foundation and the American Society of Civil Engineers. Held at the Cresta Sun Hotel in Davos, Switzerland, from May 25-30, 1997, the conference was organized by the Imaging Technologies Committee of the Technical Council on Computer Practices of the ASCE. The conference provided an opportunity to continue the technical interaction initiated during the First International Conference held in Hawaii in March, 1993. The Davos meeting agenda included topics ranging from material characterization, deformation measurements, pavement distress, infrastructure maintenance, object

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FOREWORD

The Engineering Foundation and the National Science Foundation co-sponsored a conference entitled "Digital Image Processing: Techniques and Applications in Civil Engineering" that was held in Hawaii in March, 1993. The purpose of the conference was to provide an opportunity for researchers and practitioners from academia, government and industry to convene and exchange information and ideas. Despite the fact that there were a significant number of people beginning to use image processing techniques in a range of civil engineering applications at that time, there had never been a meeting of the type held. The conference thus provided an efficient means for transfer of information between those already actively using the technology, as well as to inform those considering use of digital image processing of the potential benefits. The proceedings of the conference were published by ASCE in 1993.

To facilitate continued exchange of information and ideas, the Second International Conference on Imaging Technologies: Techniques and Applications in Civil Engineering was held in Davos, Switzerland in May, 1997. As with the first meeting, the intent was to create an opportunity for practitioners and academicians from a variety of agencies to learn of continued developments and applications in the field. As with all Engineering Foundation conferences, the meeting agenda included significant opportunities for ad-hoc discussion among the participants as well as more structured sessions with presentations of technical papers submitted by participants in topics ranging from material characterization, deformation measurements, pavement distress, infrastructure maintenance, object recognition, particle sizing and image generation.

The opening keynote lecture was given by Professor Murat Kunt from the Swiss Federal Institute of Technology in Lausanne. His presentation entitled "Image Coding: From Pixels to Objects" provided an excellent summary of classical compression techniques as well as a glimpse of where the field is headed, particularly with respect to dynamic coding techniques.

Contents

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Graduate Research Assistant and Associate Professors, respectively, Georgia institute of

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SIZE DISTRIBUTION MEASUREMENTS OF MICROBUBBLES

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Application of Digital Image Analysis for Size Distribution Measurements of Microbubbles

Susan E. Burns¹, Sotira Yiacoumi¹, J. David Frost¹, and Costas Tsouris²

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 $\overline{}$ This work employs digital image analysis to measure the size distribution ition processes. Microbubbles are used for separations in the mineral \leq The primary focus of this study was to characterize the size and size ution of bubbles generated in electroflotation using image analysis. The study that bubble diameter increased slightly as the current density applied to the $\frac{1}{5}$ in was increased. Additionally, electroflotation produces a uniform bubble size arrow distribution which optimizes the removal of fine particles from solution. Electroflotationssing industry and also in the treatment of potable water and wastewater. As ibbles move upward in a solid/liquid column due to buoyancy, particles collide processeshere they iaffected by the bubbles. In general, higher separation is achieved by a smaller bubble

$\frac{\text{in}}{\text{in}}$ strongly affection

Many environmental and industrial treatment processes rely on the separation $\frac{1}{\sqrt{2}}$ d particles from liquid solutions. Traditionally, solid particles are removed by $\frac{1}{2}$ antation; however, sedimentation does not work well for low density particles $\frac{\delta}{\delta}$ ay minerals, spores, and coagulated fulvic acids (Edzwald et al., 1992; Malley $\frac{\omega}{\omega}$ azwald, 1991; Letterman, 1987). As a result, a met \mathbb{P} and \mathbb{P} are separate vironment processes relatively separation processes in the separation of \mathbb{P} floats rather than sediments low density particles, is being used more only. In flotation, small gas bubbles are generated at the bottom of the water a to be treated. The microbubbles then rise to the surface of the liquid through

general, higher separation is achieved by ^a smaller bubble

solution; consequently, the low density solids are floated to the top of the column for removal by skimming. The process of flotation is known as dissolved air flotation if the microbubbles are produced by pressurizing air into water, as dispersed air flotation if the bubbles are produced by forcing gas through a sparger, and as electroflotation if the bubbles are produced through the electrolysis of water. This study will focus on bubbles generated by electroflotation.

Electroflotation has been used by the mineral processing industry for the consequently consequently industrial processes for the conception of oil function ϵ . industrial processes for the separation of oil from oil/water emulsions (Hosny, 1992; microbubbles and Foulds, 1986), and for the removal of coagular

produced by pressuring and the water, and the coagular contract and the contract of the contr solution (Srinivasan and Subbaiyan, 1989; Ramadorai and Hanten, 1986). In all of these applications, the removal efficiency is strongly affected by the size of the generated bubbles. Smaller bubbles have a longer residence time in the system, have a larger surface area, and are more likely to adhere to solids after a collision (de Rijk et al., 1994). Consequently, the treatment process is optimized by generating the smallest diameter bubbles possible.

This paper examines the effect of the process variable $\frac{S}{\text{by}}$ and ionic strength on the size of the bubbles generated of μ bubble images were recorded with a long-distance, high-ma and were printed and imported into a digital image analysis system for measurement of equivalent bubble diameter. The average equivalent circular diameter for was The study or equivalent bubble diameter. The average equivalent circle solid to the calculated for each experimental condition; additionally, the pubbles is the bubbles was colouleted for each experiment \mathbf{p} the bubbles

Experimental effect of the process variables of voltage, current, current

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and ionic strength on the size of the size of the bubbles generated during electroflotation. The size of the bubbles generated during electroflotation. The size of the bubbles generated during electroflotation. The size o $\mathbf{p}_{\text{intra}}$ The rectangular test cell used in the experiments of α longwith—dimensions of ϵ 0.4 P exigles with dimensions of 58.4 cm by 7.6 cm by 2.5 cm ports were drilled in the top and bottom of the cell and it was mounted vertically in order to allow gas flow out the top. After the cell was filled with the test solution, a soap-film flow meter was attached to one outflow port to measure gas flow rate and the remaining outflow ports were sealed. The electrodes used in the experiments were polished graphite electrodes (7.6 cm by 2.5 cm by 1.3 cm) and were mounted at the bottom of the cell with a separation of 13 cm. Electrical leads were attached to $\frac{1}{2}$ in the electrones using conductive epoxy, and then connected supply.

> in the top and both the top and the top and the top and the control and it was more than Γ Equilibrium of the top of the top of the top of the test solution of the cell was defining determined with Na $SO_{1,1}$ at ionic strengths of 0.1 deionized water mixed with Na_2SO_4 at ionic strengths of 0.1, 0.01, and 0.001 M. In the experiments, the voltage was varied from 15 to 86 V and the current was varied $\frac{1}{2}$ current now 2.68 mA. Current was applied to the system using current now and we concerned by the concerned at $\frac{1}{2}$. current power supply and the generated bubbles were videotaped using a long-

eight experiments were performed using aqueous solutions of

liquid solutions. The Research Assistant and Associate Professors, respectively, George are removed by School of Civil and Environmental Equipmentations. ren Assistant and Associate Professors, respectively, Georgia
ool of Civil and Environmental Engineering, Atlanta, GA cal Technology Division, Oak Ridge National Laboratory, P.O. Box $\mathbf{1926}$ ge, IN

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nce microscope with a magnification of approximately 230 times attached to a camera, monitor, and VCR. The calibration factor was a wire of known eter. The experiments performed at 0.001 M did not produce a significant gas rate; consequently, only the results for the experiments performed at 0.1 and M are reported in this paper.

 \blacksquare The gas bubbles produ r by the following redox reactions:

$$
H_2O \to 2H^+ + \frac{1}{2}O_2(g) + 2e^-
$$
 Anode(+)
\n
$$
2H_2O + 2e^- \to 2OH^- + H_2(g)
$$
 Cathode(-)

^a magnification of approximately ²³⁰ times attached to ^a

 $\frac{1}{\pi}$ oxygen and hydrogen gas dissolve into the liquid surrounding the electrodes; $\frac{1}{2}$ bubbles produced in electronics superstandanced with gas, bubbles elegan to form on the electronics of the electrolysis of the elec $\frac{1}{2}$ for $\frac{1}{2}$ and $\frac{1}{2}$ redox reactions: $\frac{1}{2}$ redox reactions: $\frac{1}{2}$ rea Figure 1.1 The electrical leads were reversed making the bottom electrode the α ode. This configuration was used because it prevented the mixing of oxygen and $\overline{\vec{a}}$ and the solution in the recorded images. \mathbf{d} the cell to \mathbf{d}

ge Processing and Analysis

 \leq Aft fter the experiments were completed, the images were printed to hard continued to 6570 . Districted Images $\frac{dS}{dt}$ g a video copy processor and imported into a Quantimet Q570 Digital Ima essor. The printed images were gray-scale pictures of dark bubbles on a light bubbles during video the grap set up behind the cell was blocked by the bubbles but
a light source behind the cell was blocked by the bubbles but ed through the aqueous solution. After the images were acquired by the ima and $\frac{1}{2}$ and $\frac{1}{2}$ and $\frac{1}{2}$ are surfacent of the electrode. Average or the electrode. Average of the electrode. Average of the electrode. As $\frac{1}{2}$ and $\frac{25}{2}$ and $\frac{25}{2}$ and $\frac{25}{2}$ and $\frac{25}{$ $\frac{1}{2}$ hed each other on the images. In this case, the bubbles were either separated and $\frac{\Delta T}{\Delta 0}$ yzed individually, or were eliminated from the image. No other image lessing was performed on the bubble pictures. Because not all of the bubbles e circular in cross-section, the image analyzer measured the area of each bubble converted that to an equivalent circular diameter for the output. essor, they were converted from gray-scale into digital images and a minimal $\frac{1}{2}$ bubbles $\frac{1}{2}$

e converted from gray-scale into digital processingor in the measurement. Measurements of one experiment were performed twice the difference was 1.9 µm between the average diameters measured. Assuming a $\frac{1000}{1000}$ and distribution, and choosing a 95 % confidence interv culated by the following (Hines and Montgomery, 1990):

cross=section, the image analyzer measured the area of each bubble analyzer measured the area of each bubble

statically valid sample size was chosen for anaiysis by first determining the

converted that to an equivalent circular diameter for the output.

$$
a = \left(\frac{Z_{\alpha/2}\sigma}{E}\right)^2,\tag{1}
$$

where $n =$ sample size, $Z_{\alpha/2} =$ confidence interval, $\sigma =$ standard deviation, and $E =$ error.

<u>Results</u>

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AverageBubble Diameter (F

le size,

Figure 1 shows a plot of the equivalent circular diameter of oxygen bubbles
as a function of current density. The figure shows a trend of slightly increasing
bubble diameter with increasing current density applied to the s lectrodes; consistent with other electroflotation results using metallic e Exploration interval, and the electronomic measures using metallic
Kelsall, 1985; Janssen and Hoogland, 1973; Landolt et al., than a homogeneous process where the bubbles form out of solution without the shows ^a ^plot of the equivalent circula ' . ^r diameter of oxygen bubbles Glas and Westwater, 1964) which illustrates the importance of the surface characteristics of the electrodes. In this study, the electrodes were not polished between successive experiments which most likely explains the scatter seen in the average bubble diameter measurements, because the application of current will affect average bubble diameter measurements, because the application
the surface characteristics of the electrode. Average oxygen electrode. Average oxygeneous is an inhomogeneous controlled process rather than in the experiments ranged from 171 $\frac{1}{2}$ diameters measured in the experiments ranged from 17.1 of a surface a surface a surface of surface a surface of surface and the size of bubbles produced on stainle

electrodes (Ketkar et al. 1991) electrodes (Ketkar et al., 1991).

Figure 1. Oxygen bubble diameter as a function of current density: $I = 0.1 M$.

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