

VOLUME 39 / NUMBER 4 / FEBRUARY 20, 1992

BIO TECHNOLOGY & BIOENGINEERING

EDITOR

ELEFThERIOS T. PApOUTSAKIS

DOCKET
ALARM

Find authenticated court documents without watermarks at docketalarm.com.

Editor
Eleftherios T. Papoutsakis
Northwestern University, Evanston, Illinois

Associate Editors
Douglas S. Clark, *University of California
Berkeley, California*
C. P. Leslie Grady, Jr., *Clemson University
Clemson, South Carolina*
Maria-Regina Kula, *Heinrich-Heine Universität Düsseldorf
in der KFA Julich, Germany*
Daniel I. C. Wang, *Massachusetts Institute of Technology,
Cambridge, Massachusetts*

Scope: The Editors of *B&B* will consider for publication original articles and mini reviews that deal with all aspects of applied biotechnology. These include:

- applied aspects of cellular physiology, metabolism, and energetics of bacteria, fungi, animal, and plant cells;
- enzyme systems and their applications, including enzyme reactors, purification, and applied aspects of protein engineering;
- animal-cell biotechnology, including media development, modeling, tissue engineering, and applied aspects of cell interactions with their environment and other cells;
- bioseparations and other downstream processes including cell disruption, chromatography, affinity purifications, extractions, and membrane processing;

Biotechnology and Bioengineering (ISSN:0006-3592) is published 22 times per year, semi-monthly, except May, July, September, and November, when it is published monthly, and in March and April when it is published 3 times, on the 5th, 15th, and 25th, by John Wiley & Sons, Inc., 605 Third Avenue, New York, NY 10158.

Copyright © 1992 by John Wiley & Sons, Inc. All rights reserved. Reproduction or translation of any part of this work beyond that permitted by Sections 107 and 108 of the U.S. Copyright Law without the permission of the copyright owner is unlawful. Second-class postage at New York, NY, and additional mailing offices.

The code and copyright notice appearing at the bottom of the first page of an item in the journal indicates the copyright holder's consent that copies may be made for personal or internal use, or for the personal or internal use of specific clients, on the condition that the copier pay for copying beyond that permitted by Sections 107 or 108 of the United States Copyright Law. The percopy fee for each item is \$4.00 and is to be paid through the Copyright Clearance Center, Inc., 21 Congress St., Salem MA 01970. This consent does not extend to other kinds of copying, such as copying for general distribution, for advertising or promotional purposes, for creating new collective works,

- environmental biotechnology, including aerobic and anaerobic processes, systems involving biofilms, algal systems, detoxification and bioremediation, and genetic aspects;
- applied genetics and metabolic engineering, including modeling molecular processes of applied interest;
- plant-cell biotechnology;
- biochemical engineering, including transport phenomena in bioreactors, bioreactor design, kinetics and modeling of biological systems, instrumentation and control, biological containment, and bioprocess design;
- biosensors;
- spectroscopic and other instrumental techniques for biotechnological applications, including NMR and flow cytometry;
- thermodynamic aspects of cellular systems and their applications;

or for resale. Such permission requests and other permission inquiries should be addressed to the Permissions Dept.

Subscription price (1992): Volumes 39 & 40, 22 issues: \$950.00. Outside U.S.A.: \$1225.00 (includes air service and handling). Back volumes, microfilm, and microfiche are available for previous years; request price list from the publisher. Please allow 4 weeks for processing a change of address. For subscription inquiries, call customer service at (212) 850-6645 or write to the above address.

Claims for undelivered copies will be accepted only after the following issue has been received. Please enclose a copy of the mailing label or cite your subscriber reference number in order to expedite handling. Missing copies will be supplied when losses have been sustained in transit and where reserve stock permits.

Postmaster: Send address changes to *Biotechnology and Bioengineering*, Susan Malawski, Fulfillment Manager, Subscription Department, John Wiley & Sons, Inc., 605 Third Avenue, New York, NY 10158.

Advertising Sales: Inquiries concerning advertising should be forwarded to Roberta Frederick,

Founding Editor
Elmer L. Gaden, Jr., *University of Virginia,
Charlottesville, Virginia*

Editorial Board
James E. Bailey
Harvey W. Blanch
Arnold L. Demain
Isao Karube
Malcolm D. Lilly
Michael L. Shuler
Daniel Thomas

- mineral biotechnology, including coal biotechnology;
- biological aspects of biomass and renewable resources engineering; and
- fundamental aspects of food biotechnology.

The editors will consider papers for publications based on novelty, their immediate or future impact on biotechnological processes, and their contribution to the advancement of biochemical engineering science. Submission of papers dealing with routine aspects of bioprocessing, description of established equipment, and routine applications of established methodologies (e.g., control strategies, modeling, experimental methods) are discouraged. Theoretical papers will be judged based on the novelty of the approach and their potential impact, or on their novel capability to predict and elucidate experimental observations.

Advertising Sales, John Wiley & Sons, 605 Third Ave., New York, NY 10158; (212) 850-8832. Advertising Sales, European Contact: Michael Levermore, Advertising Manager, John Wiley & Sons, Ltd., Baffins Lane, Chichester, Sussex PO19 1UD, England.

Manuscripts should be submitted to the *B&B* Editor, Professor Eleftherios T. Papoutsakis, Dept. of Chemical Engineering, Northwestern University, 2145 Sheridan Rd., Evanston, IL 60208-3120, USA.

All Other Correspondence: Address to *Biotechnology & Bioengineering*, Publisher, Inter-science Division, Professional Reference, and Trade Group, John Wiley & Sons, Inc., 605 Third Ave., New York, NY 10158.

Information for contributors appears in the first and last issue of each volume. The contents of this journal are indexed or abstracted in the following: *Biological Abstracts; Chemical Abstracts; Chemical Titles; Current Awareness in Biological Sciences; Current Contents/Life Sciences; Current Contents/Engineering Technology and Applied Sciences; Excerpta Medica; and Science Citation Index.*

Editorial Production, John Wiley
Hattie Heavner and Don Simmons, Jr.

Cell Immobilization Using PVA Crosslinked with Boric Acid

Kuo-Ying Amanda Wu and Keith D. Wisecarver*

Department of Chemical Engineering, The University of Tulsa,
Tulsa, Oklahoma 74104

Received July 18, 1991/Accepted July 26, 1991

A new cell immobilization technique is described in which polyvinyl alcohol is crosslinked with boric acid, with the addition of a small amount of calcium alginate. The presence of the calcium alginate improves the surface properties of the beads, preventing agglomeration. A pure culture of phenol-degrading *Pseudomonas* was immobilized in the PVA-alginate beads. Phenol was successfully degraded in a fluidized bed of the beads, indicating that cell viability was maintained following the immobilization procedure. The PVA-alginate beads proved to be very strong and durable, with no noticeable degradation of the beads after 2 weeks of continuous operation of the fluidized bed.

Key words: immobilized cell • PVA • polyvinyl alcohol • fluidized bed

INTRODUCTION

Immobilization of living cells has become an established technique for increasing the productivity of biochemical engineering processes. One of the most widely used techniques for cell immobilization is cell entrapment, in which the living cells are enclosed in a polymeric matrix which is porous enough to allow the diffusion of substrates to the cells and of products away from the cells. Materials which have been successfully used for cell entrapment include agar, agarose, kappa-carragennan, collagen, alginates, chitosan, polyacrylamide, polyurethane, and cellulose.⁹ However, each of these polymers has drawbacks, such as poor mechanical strength and durability (agar, agarose, kappa-carragennan, collagen, alginates, chitosan), toxicity to microorganisms (polyacrylamide, polyurethane), or high cost.^{1,5}

Recently, the use of polyvinyl alcohol (PVA) for cell immobilization has been investigated. Ariga et al.¹ used the technique of iterative freezing and thawing of PVA to form a gel suitable for cell immobilization. They found that this technique produced a low-cost material with a rubber-like elasticity and high strength. Hashimoto and Furukawa³ used a simpler and less energy-intensive

duced by other cell immobilization techniques such as polyacrylamide and calcium alginate.¹

The PVA-boric acid technique provides an easy and low-cost method of cell immobilization, producing elastic beads of high strength and durability.³ There are two potential problems with this technique, however. The saturated boric acid solution used to crosslink the PVA is highly acidic (pH of approximately 4) and thus could cause difficulty in maintaining cell viability. Hashimoto and Furukawa³ hypothesized that activated sludge could be successfully immobilized without loss of biological activity due to the presence of extracellular polymer in the sludge, which enables the microorganisms to endure changes in cultivation conditions, and cast doubt on whether the technique could be applicable for other types of cells. To date, the use of the PVA-boric acid immobilization technique for other types of microorganisms has not been demonstrated. In addition, PVA is an extremely sticky material; PVA beads, therefore, have a tendency to agglomerate. This is particularly a problem in applying PVA-immobilized cells to fluidized bed reactors. The elasticity and high strength of the PVA beads are ideally suited to the high shear stresses encountered in fluidized beds,¹ but the tendency of PVA beads to agglomerate can make fluidization difficult or impossible.

In this article, a new cell immobilization technique is described which eliminates the agglomeration problem of the PVA-boric acid method by the addition of a small amount of calcium alginate. The technique was demonstrated for a pure culture of *Pseudomonas*. The resulting beads were utilized in a three-phase fluidized bed bioreactor to demonstrate viability of the immobilized cells.

MATERIALS AND METHODS

The microorganisms used in this work was a pure strain

Trace elements include (mg/L): zinc, 0.01; copper, 0.001; selenium, 0.001.

OD (460 nm) of approximately 1.1, a period of approximately 24–30 h, at which time they were centrifuged at 1000 rpm for 10 min.

The cell immobilization process is illustrated in Figure 1. Water was added to 43.7 g of polyvinyl alcohol (100% hydrolyzed, average MW 77,000 to 79,000) to obtain 330 mL of solution. The solution was then carefully heated to a temperature of 60°C to completely dissolve the PVA. A solution of 3.5 mL of 2% sodium alginate (low viscosity, approximately 250 cps) in water was prepared by gently stirring for 30 min and added to the PVA solution. The PVA-alginate solution was then cooled to a temperature of 35°C.

The centrifuged cells (45.6 g wet weight) and 35 mL of distilled water were mixed with 6.3 mL of the growth medium (Table I) to supply nutrients for the microbial

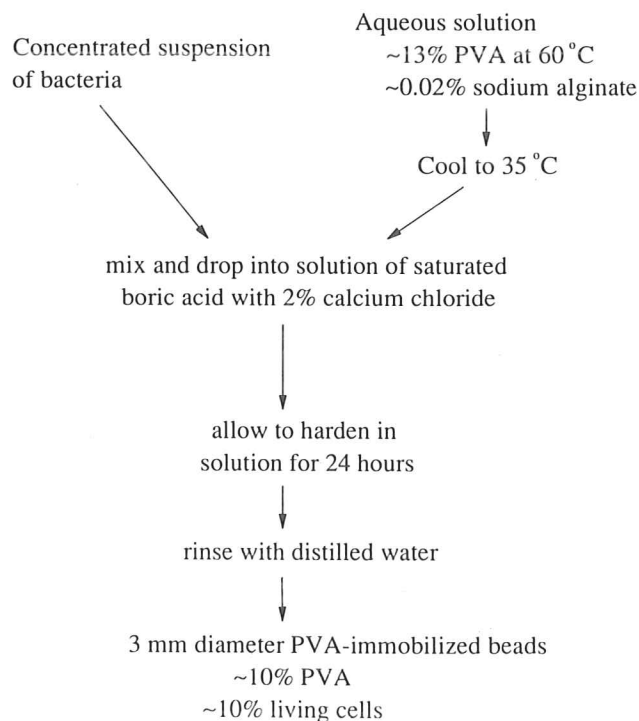


Figure 1. Cell immobilization using PVA-boric acid with calcium alginate.

stirred in this solution for 24 h to complete the solidification, and then rinsed with distilled water to remove any excess boric acid. Approximately 420 cm³ of bead containing the immobilized cells were thus formed. The diameter of the beads was approximately 3 mm.

Cell viability and bead integrity were tested in an 8-l fluidized bed column. The 10.16 cm ID column was sparged with air at a rate of 1.4 L/min. Growth medium (Table I), containing varying concentrations of phenol was fed continuously from the top of the column, and effluent withdrawn at the column bottom, at a rate of 2.5 L/h. The fluidized bed experiments were conducted at room temperature.

Phenol concentrations of all the samples in this work were analyzed by gas chromatography⁸ (Hewlett Packard model 5890A with flame ionization detector).

RESULTS AND DISCUSSION

Initial attempts at cell immobilization were made using only PVA crosslinked with boric acid. However, the beads thus formed had a strong tendency to agglomerate into a mass of polymer which was very difficult to break up. The beads could, therefore, not be utilized in a fluidized bed. This agglomeration problem appears to be due to the relatively slow crosslinking of the PVA by boric acid. Droplets of PVA, which have not been sufficiently crosslinked, tended to agglomerate into a mass. This problem persisted even with vigorous stirring of the boric acid solution to keep the beads suspended.

Attempts were then made to use a combination of PVA-boric acid and calcium alginate, by hardening a mixture of PVA and sodium alginate with a mixed solution of boric acid and calcium chloride. In this way, it was thought that the PVA might contribute durability and strength to the beads, while calcium alginate might improve the surface properties of the beads, reducing the tendency to agglomerate. The percentage of PVA in the beads was kept in the range of 10% to 12.5%, as recommended by Hashimoto and Furukawa,³ to maintain maximum bead strength. Varying ratios of dry PVA to 2% sodium alginate solution were attempted for the immobilization procedure. It was found that agglomeration of the beads was entirely prevented for PVA to alginate solution ratios of 5:1, 8:1, 10:1, and 12.5:1, while agglomeration persisted for a 20:1 ratio. The 12.5:1 ratio (43.7 g PVA to 3.5 mL of 2% sodium

alginate), which corresponds to a total alginate concentration in the beads of approximately 0.02%, was concluded to be approximately the lowest concentration of alginate that would prevent bead agglomeration. It is theorized that calcium alginate is formed nearly instantaneously when the sodium alginate solution contacts the calcium chloride solution, and that the resulting polymeric structure is sufficient to keep the beads from agglomerating during the PVA crosslinking process. The resulting beads were strong and highly elastic, and of early spherical shape.

Fluidized bed experiments were conducted continuously over a period of 2 weeks. Inlet phenol concentration was increased in steps from 250 to 1300 mg/L (inlet phenol concentrations of 250, 350, 450, 550, 650, 750, 850, 950, 1000, 1100, 1200, and 1300 mg/L were used), with the bioreactor allowed to achieve steady state between each step increase. This range was chosen to be close to the range of phenol concentrations to which the microorganisms had been acclimated. The steady-state outlet phenol concentration, measured by gas chromatography, was found to be zero for each of these inlet phenol concentrations.

Phenol removal due to stripping was measured by diverting the off-gas from the column through a NaOH solution (pH 10) and measuring the absorbed phenol. The phenol removed by stripping was found to be less than 0.1% of the total phenol degradation. Bioadsorption has been found by a number of investigators to be small in comparison with biodegradation.^{2,4,7} Therefore, it can be concluded that phenol removal in the fluidized bed was due almost entirely to biodegradation, indicating that cell viability was maintained through the immobilization procedure.

The bioparticles made from the PVA-alginate immobilization technique proved to be very durable, showing no sign of breakage or disintegration after 2 weeks of continuous operation of the fluidized bed. The PVA-alginate beads showed no tendency to agglomerate at

any time during the fluidized bed experiments. Measurements of bead size, before and after the fluidized bed experiments, showed no discernable difference.

CONCLUSIONS

Immobilization of living cells of a phenol-degrading *Pseudomonas* isolate in a PVA-boric acid gel was demonstrated. Cell viability was indicated by degradation of phenol in a fluidized bed reactor of the beads. The presence of a small amount of calcium alginate in the beads, as small as 0.02%, was shown to prevent agglomeration of the PVA beads. The resulting beads were highly elastic and durable; they were able to withstand high shears in a three-phase fluidized bed for 2 weeks of continuous operation with no noticeable breakage or shrinkage of the beads. The successful immobilization of a *Pseudomonas* isolate by the PVA-boric acid method indicates that the technique might be applicable to a wide variety of microorganisms.

References

1. Ariga, O., Takagi, H., Nishizawa, H., Sano, Y. 1987. *J. Ferment. Technol.* **65**: 651.
2. Gaudy, A. F., Kincannon, D. F., Manickam, T. S. June 1982. EPA-600/2-82-075.
3. Hashimoto, S., Furukawa, K. 1987. *Biotechnol. Bioeng.* **15**: 52.
4. Kincannon, D. F., Stover, E. L., Nichols, V., Medley, D. 1983. *J. Water Pollut. Control Fed.* **55**: 157.
5. Kuu, W. Y., Polack, J. A. 1983. *Biotechnol. Bioeng.* **25**: 1995.
6. Ochiai, H., Shimizu, S., Tadokoro, Y., Murakami, I. 1981. *Polymer* **22**: 1456.
7. Petrasek, A. C., Kugelman, I. J., Austern, B. M., Pressley, T. A., Winslow, L. A., Wise, R. H. 1983. *J. Water Pollut. Control Fed.* **55**: 1286.
8. Standard methods for the examination of water and wastewater, 16 ed. 1985. American Public Health Association, Washington, DC.
9. Tampion, J., Tampion, M. D. 1987. *Immobilized cells: Principles and applications*, Cambridge University Press, Cambridge, UK.