UNITED STATES PATENT AND TRADEMARK OFFICE

BEFORE THE PATENT TRIAL AND APPEAL BOARD

UMICORE AG & CO. KG,

Petitioner

Patent No. 7,601,662 Issue Date: October 13, 2009 Title: COPPER CHA ZEOLITE CATALYSTS

DECLARATION OF Dr. FRANK-WALTER SCHÜTZE

Case No. IPR2015-01121



I, Dr. Frank-Walter Schütze, declare as follows:

I. BACKGROUND

- 1. I am currently a Senior Manager R&D / Strategic Projects and I am involved in SCR research and development as well as zeolite related topics in connection with automotive catalysts at Umicore AG & Co. KG ("Umicore"), which is located in Hanau-Wolfgang, Germany.
- 2. I studied chemistry at the University of Leipzig (Germany) and received my Ph.D. in Chemistry in 1997. From 1997 to 2001, I was a post doc researcher at the University of Oldenburg (Germany) and the Institute of Applied Catalysis Berlin (Germany).
- 3. I have held my current position at Umicore since the 1st of January 2015. Prior to that, I was Senior Manager R&D / Research and Customer Projects and was involved in SCR / ASC development. Since I joined Umicore in 2001, I was involved in R&D for automotive catalysts on several topics, very often related to application of zeolites in catalyst formulations.

II. ASSIGNMENT

- 4. I was asked to make samples of copper-loaded chabazite zeolite ("Cu-CHA") catalysts with varying silica to alumina molar ratios (which I will refer to as the "SAR") and copper to aluminum atomic ratios (which I will refer to as the "Cu/Al ratio").
 - 5. I was asked to test the catalyst samples I made in different ways. In



particular, I was asked to assess each sample's effectiveness at catalyzing the reduction of nitrogen oxides in a gas stream both before and after hydrothermal aging.

III. MATERIALS TESTED

- 6. I started my preparation of Cu-CHA catalyst samples by obtaining various ammonium-type chabazite zeolite (NH₄-CHA) materials with different framework SARs. I obtained chabazite materials with SARs of 13, 19, 21, 27, and 30.
- 7. Next, I copper-loaded these various NH₄-CHA materials to produce Cu-CHA zeolite samples with different Cu/Al ratios ranging from 0 to 1. Copper-loading of the NH₄-CHA materials was performed by aqueous ion-exchange. The required amount of copper-acetate needed to produce a given Cu/Al ratio was mixed with the NH₄-CHA and the suspension was then heated for 2 hours at 65 °C.
- 8. For the creation of recipes related to the targeted Cu/Al ratios for CHA materials with the different SAR, I have used molar relationships of the components based on their direct structural correlations. Based on the SAR of the CHA material, I determined the molar composition of the so called "unit cell" (or "u.c.") of the material. The unit cell of a protonated CHA material has the formula ([Si_{36-x} Al_x O₇₂] H_x). Using this formula, the molar amount of aluminum or alumina in this structural building unit, and thus the ion-exchange capacity, can be calculated. I used the well accepted stoichiometric assumption that 1 Cu²⁺ ion balance the charge introduced by 2 Al atoms in the structural building unit.
 - 9. For example: a CHA zeolite with an SAR of 22 contains 3 moles of Al in



the framework of the unit cell, introducing 3 moles of positive charge into 1 mole of the appropriate unit cell. From this I calculated the target amount of Cu²⁺ for the appropriate ion-exchange level (using the above explained assumption) based on the molar mass of Cu (63.546 g/mole). The stoichiometric maximum amount of copper that can be ion-exchanged into a zeolite with a SAR of 22 is 1.5 mole of Cu, or 95.319 g Cu/mole CHA unit cell.

- 10. The unit cell formula for a complete stoichiometric ion-exchange is represented by ($[Si_{33}Al_3O_{72}]$ Cu_{1.5}). From this formula I have calculated (based on the molar masses of the elements in the unit cell) an amount of 4.226 wt % of Cu in the material. This is the stoichiometric maximum 100% ion-exchange corresponding to a Cu/Al ratio of 0.5.
- 11. With these correlations, I created the preparation recipes for the different CHA-catalyst samples with the different SAR values and Cu/Al ratios (or Cu and CuO concentrations, respectively). In these calculations, I determined the appropriate amount of Cu-precursor needed (Cu-acetate) to produce the desired Cu/Al ratio via ion exchange given the SAR and amount of zeolite in the ion-exchange slurry.
- 12. When calculating the Cu/Al ratios of the materials I prepared, I was asked to include only the aluminum from the zeolite and ignore any other aluminum present in the resultant catalyst material, including any aluminum from the binder or other sources.



- 13. I then coated these Cu-CHA zeolite materials onto ceramic cordierite substrates with a cell density of 400 cpsi (cells per square inch) and a wall thickness of 6.5 mil. The substrates had either a 3.66 or 5.66 inch diameter, and a length of 3 inches. To improve the adhesion properties of the Cu-CHA zeolite to the substrate, a binder was used in an amount of 12 wt %, resulting in an overall washcoat loading amount of 150 g/L coated catalyst volume. After coating, the substrates were dried and calcined. The catalysts with a SAR of 13 were calcined for 2 hours at 500 °C in air, while the other catalysts were calcined for 4 hours at 640 °C in air.
- 14. In addition to the Cu-CHA zeolite coated substrates, I was also asked to make a number of copper loaded beta zeolite (BEA) coated substrates. To create these samples, I used a BEA zeolite with a SAR of 30, which I copper loaded using the same procedure described above to produce Cu/Al ratios in the range of approximately 0.15 to 0.55. I then coated substrates with the copper loaded BEA zeolite material in the same manner I describe above for the Cu-CHA materials.
- 15. Then multiple 1 inch diameter x 3 inch length core samples were drilled out of each Cu-CHA coated substrate to allow for testing. A fresh core sample was retained from each Cu-CHA coated substrate. And, a core sample from each Cu-CHA coated substrate was aged for 50 hours at 800 °C using a forced flow-through of hydrothermal atmosphere containing 10 vol. % of oxygen and 10 vol. % of water vapor balanced by nitrogen. This treatment is assigned as 50 B 800 in the attached exhibits.



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